

IN THE SPECIFICATION

Change the title of the present invention to: A BIOREACTOR PROCESSING METHOD
WITHIN A TANK INTERNALLY CHAMBERED TO SEQUENTIALLY PERFORM
BIOLOGICAL TREATMENT AND MEMBRANE FILTRATION.

Please replace the paragraph inserted after paragraph numbered [0002] with the following paragraph:

CROSS-REFERENCE TO RELATED APPLICATION

[0002A] This application ~~claims the benefit~~ is a divisional application of U.S. Non Provisional Application No. 10/263,286 filed Sept. 25, 2002, entitled "A BIOREACTOR TANK INTERNALLY CHAMBERED TO SEQUENTIALLY PERFORM BIOLOGICAL TREATMENT AND MEMBRANE FILTRATION", incorporated herein by reference.

Please replace paragraph numbered [0005] with the following paragraph:

[0005] In accordance with the present invention, a single tank ~~is utilized in~~ of a bioreactor system~~[[,]]~~ is internally partitioned into a volumetrically large chamber within which biological treatment of a fluent biomass such as wastewater contaminated by solids suspended therein, is continuously performed, and a volumetrically small chamber within which membrane filtration is performed after the treated wastewater collected within the small chamber undergoes separation between portions thereof by a dewatering device, located outside of the tank. Separation of such portions of the wastewater respectively increases and lowers contamination so that the portion

with lowered contamination may undergo the filtration into a cleansed effluent to be withdrawn[[,]] . ~~reflective of~~ Such system involves maximized removal of suspended solids during processing of the wastewater contaminated under different conditions. Selectively controlled valve means is associated with the system in order to interrupt performance of the membrane filtration ~~performed~~ within the small chamber of the tank, while the separated portion with increased contamination is continuously recycled into the large chamber for biological retreatment. Also, some of the separated portion of the wastewater with the lowered contamination is disposed of by direct discharge ~~from~~ through the dewatering device in by-pass relation to the tank, when the contamination condition does not require membrane filtration.

Please replace paragraph numbered [0009] with the following paragraph:

[0009] Referring now to the drawing in detail, apparatus of a bioreactor system 10 is illustrated in FIG. 1, involving use of a single collection tank 12 ~~to~~ into which a contaminated fluent biomass, such as raw feed streams of non-oily wastewater, is fed through an inlet 14 under pressure of a pump 16 from sources 17, such as showers, sinks, toilets and urinals on-board a sea vessel for example, within which the system 10 may be installed. Such wastewater feed streams enter ~~the~~ a top 13 of the tank 12 through the inlet 14 for collection therein on opposite sides of a weir plate 18 internally partitioning the tank 12 into a volumetrically smaller chamber enclosing an assembly 20 of membranes immersed within wastewater having its contamination lowered and a larger volume chamber within which aeration by an aerator 19 promotes biological treatment. The wastewater with a lowered concentration of contamination solids inside the smaller chamber is filtered by permeation through the membranes of the assembly 20, under suction applied by a

pump 22, to withdraw a permeate as a cleansed effluent, having substantially little or no contaminating solids therein. Biologically treated wastewater is recycled under pressure of a pump 28 from a bottom 27 of the larger chamber into the smaller chamber through a dewatering device 24, from which a portion of the wastewater with the solids concentration lowered is separated from another portion with an increased solid concentration as a result of centrifugation. The pump 28 withdraws the biologically treated wastewater from the bottom 27 of the larger volume chamber of the tank 12 underlying ~~an~~ the aerator 19, so as to recycle the biologically treated wastewater ~~along a path~~ outside the tank 12 through the dewatering device 24 for delivery of the separated portion thereof with the lowered solids concentration through a valve 29 into the smaller volume chamber of the tank 12, within which it undergoes membrane permeation. The wastewater portion having the increased solids concentration separated by the dewatering device 24 from the lowered solids concentrated wastewater portion, is continuously returned through a recycling conduit 26 from the dewatering device 24 into the larger volume chamber so as to elevate the suspended solids concentration therein, which undergoes biological retreatment. The wastewater undergoing such recycling, is maintained at a surface level within the larger chamber lower than that in the smaller volume chamber, ~~from which the~~ as shown in FIG. 1. The wastewater within the smaller volume chamber accordingly overflows the weir plate 18 into the larger volume chamber as indicated by the curved arrow 21. By the membrane permeate filtration within the smaller tank chamber, the solids are finely separated therein, and withdrawn therefrom by the pump 22. The in-feed flow rate of wastewater into the tank 12 through the inlet 14 allows the aforementioned overflow 21 of the wastewater into the larger volume chamber, within which the wastewater surface ~~level~~ is maintained at a the lower level below the top of the

weir plate 18, as shown in FIG. 1. By virtue of aeration within the larger volume chamber of the tank 12 by the aerator 19, aerobic bacterial growth is promoted during biological treatment so as to enhance the permeation through the membranes in the assembly 20 to more fully cleanse the wastewater being withdrawn by the pump 22 as an effluent.

Please replace paragraph numbered [0010] with the following paragraph:

[0010] The contamination of the wastewater to be processed, will depend upon the condition of the seawater through which a sea vessel travels, when the bioreactor system 10 is installed therein. With the seawater under restricted or regulated conditions during location of the sea vessel near shore for example, processing may not require or call for membrane filtration. Since processing by the bioreactor system 10 involves exposure of the wastewater after biological treatment in the large chamber to ultraviolet radiation by the aerator 19, system size and tank volume requirements are thereby reduced while successfully processing wastewater contaminated by a high solids concentration within the tank 12. Also, clarification of the collected wastewater at its expected and achievable delivery inflow rate into the tank 12 through the inlet 14, will be dependent upon the number of membranes within the assembly 20, which may accordingly be selected in order to accommodate needs such as the size of a crew on-board the sea vessel.

Please replace paragraph numbered [0011] with the following paragraph:

[0011] Because of the aforesaid lowering of solids concentration of a separated portion of the wastewater during passage through the dewatering device 24, the other separated portion of the wastewater with increased solids concentration is recycled by the pump 28 into the large

chamber to undergo biological retreatment. Membrane permeation within the small chamber by the assembly 20 is thereby enhanced under certain contamination conditions of the wastewater delivered to the system 10. The recycling of wastewater into the small chamber through the valve 29 is interrupted under selective control as hereinafter explained, when filtration is not required so as to reduce membrane fouling within the assembly 20 and thereby prolong its operational life.

Please replace paragraph numbered [0012] with the following paragraph:

[0012] While a sea vessel within which the bioreactor system 10 is installed is being propelled through seawater under the aforementioned conditions that do not require solids separation by the membrane assembly 20 in order to sufficiently cleanse the wastewater, the aforesaid interruption in filtration is achieved by closure of the valve 29 so as to operationally isolate the small membrane chamber, while a discharge valve 30 is opened by means of a control 31 as diagrammed in FIG. 1 for direct compact disposal of the separated waste sludge portion of the wastewater from the dewatering device 24 otherwise delivered to the small chamber.

Please replace paragraph numbered [0013] with the following paragraph:

[0013] In accordance with functioning of a the dewatering device 24 as generally known in the art, the aforementioned centrifugation is performed ~~within the dewatering device 24 therein~~ so as to separate the biologically treated wastewater into the two aforementioned portions, one of which has its solids concentration lowered by passage through a decanter, disk and vane-type centrifuge usually associated with dewatering devices. According to another embodiment, separation of the wastewater into the two portions involves use of dissolved air floatation by lift

of solids under pressure of wastewater in-feed and aeration injection, followed by a release of tiny air bubbles adhering to the solids in response to a drop in pressure. The solids are thereby carried in bubbles to the top surface of the wastewater within the smaller in-tank chamber to overflow the weir plate 18 into the collected wastewater within the larger volume chamber of the tank 12, maintained at its lower surface level during operation of the bioreactor system 10.

Please replace paragraph numbered [0014] with the following paragraph:

[0014] The bioreactor processing method associated with the apparatus of the bioreactor system 10, as illustrated in FIG. 1 and summarized diagrammatically in FIG. 2, involves infeed of the wastewater from the sources 17 by the pump 16 through the inlet 14 into the larger volume chamber of the tank 12 for biological treatment, after which it is recycled by the pump 28 through the dewatering device 24 to change contaminating concentration of solids by separation of the wastewater into portions thereof that are respectively returned with increased solids concentration therein into the larger volume chamber through the conduit 26 for biological retreatment, and under selective control through the valve 29 the portion with lowered solids concentration is delivered into the smaller chamber so as to undergo membrane filtration within the membrane assembly 20. Under certain contamination conditions of the wastewater being collected in the tank 12, that do not require membrane filtration, the separated portions of the wastewater are respectively returned to the large volume chamber for continued biological retreatment, and discharged directly in by-pass relation to the small volume chamber through the opened valve 30 for disposal.